EVALUATION OF THE EFFECT OF THE AIR GAP SIZE TO THE AIR DISTRIBUTION IN CHAMBER DRYING EQUIPMENT VIA CFD METHOD

ÐÁNH GIÁ ẢNH HƯỞNG KÍCH THƯỚC KHÔNG GIAN CHIA GIÓ ĐẾN PHÂN BỐ TÁC NHÂN SẤY TRONG THIẾT BỊ SẤY BẰNG PHƯƠNG PHÁP CFD

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ABSTRACT

This study evaluates the effect of the air gap size (d) on the air uniformity in the chamber dryer with the most appropriate air blade angle value inherited from the previous study. Several case studies with different values of "d" are tested. The most appropriate ratio value is 1/2; when criterion values reach the best values, show a significant improvement in the air received by the trays and the air uniformity in the equipment. Furthermore, several cases of tray and equipment length are also tested, and they also affect the air distribution.

Keywords: CFD, drying process, uniform drying, tray dryer, COMSOL multiphysics.

TÓM TẮT

Nghiên cứu đánh giá ảnh hưởng của khoảng giữa các khay và cửa gió vào đến độ đồng đều không khí trong thiết bị sấy khay dạng buồng với giá trị a thích hợp nhất được tìm thấy trong bài nghiên cứu trước. Các giá trị khác nhau đã được thử nghiệm. Tiêu chuẩn v_a, Sv, Δ v cũng được sử dụng để đánh giá độ đồng đều không khí trong thiết bị sấy. Tỉ lệ thích hợp nhất là 1/2; sự giảm của S_%, Δ v và sự tăng của v_a cho thấy sự cải thiện đáng kể về lượng không khí nhận được từ các khay và độ đồng đều của không khí trong thiết bị. Hơn nữa, một số trường hợp về chiều dài khay và chiều dài thiết bị đã được thử nghiệm, và chúng cũng có ảnh hưởng tới sự phân bố không khí trong thiết bị.

Từ khóa: CFD, quá trình sấy, sấy đồng đều, thiết bị sấy dạng khay, COMSOL multiphysics.

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1. INTRODUCTION

The drying product quality can be improved by optimizing the design of the drying equipment, with an inlet duct design [1] and inlet gap size and roof angle [2] in different types of drying equipment. The previous study only focuses on the appropriate value of angle [3], so this result does not create a totally optimal design. This study focuses on the effect of equipment dimension on product moisture homogeneity.

Meshing and setting boundary conditions significantly affect the CFD simulation results. Meshing with higher-guality unstructured meshes leads to more accurate CFD simulation but increases time and cost [4]. The meshing has to be tuned appropriately for each case study to obtain both convergence and less computational time. When dealing with complex geometries, using a combination of structured and unstructured meshes is recommended for meshing [5]. The boundary conditions need to be exactly determined for the complete description of the drying process [6].

In mesh generation, discretization error is a common problem that can reduce the

accuracy and stability of simulations. Discretization error occurs when the mesh is not fine enough to accurately represent the geometry of the problem domain. To evaluate the mesh quality, the skewness and nonorthogonality of grid elements are used as criteria [7]. Meshes with high skewness and non-orthogonality are more likely to produce inaccurate results. Adaptive mesh refinement is a common method for reducing discretization error; adaptive mesh refinement has different techniques: reducing the element size, increasing element order, etc. [8].

2. MATERIALS AND METHODS

2.1. Modeling and simulation setup

There are three main types of fluid flow: laminar flow, transitional flow, and turbulent flow, generally based on the Reynolds numbers of fluid. The Navier-Stokes equations are a set of nonlinear partial differential equations (PDEs) that govern the motion of fluids.

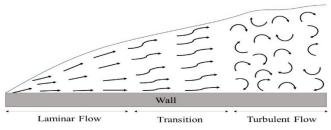


Fig. 1. Three main types of fluid flow

The Navier-Stokes equations solution is affected by two crucial factors: mesh quality and boundary conditions [9]. In turbulent flow mode, near walls, where the viscous shear stress is much stronger than the turbulent shear stress, a thin layer of fluid called the viscous layer is formed [10]. In this layer, the velocity gradient is so steep that the fluid velocity decreases to zero at the wall within a short distance. Using no-slip boundary conditions, which means fluid velocity near a wall is zero, making the velocity gradient even steeper. Slip boundary conditions allow non-zero velocity near walls, reducing the steepness of the velocity gradient and making it easier to solve.

The model and boundary conditions for simulations are set the similar as [3]. The air gap size (d) and the chamber length (l) are tuned to evaluate the effect on air distribution in this study.

2.2. Meshing method

Conforming mesh improves the accuracy of the solution near boundaries [11]. The convergence speed of the solution is highly affected by mesh quality [12].

The air blade, inlet, outlet, and material surface mainly affect the results, so they are meshed with unstructured meshes. The others are coarsely meshed to save simulation time without affecting the results. A boundary layer is a thin layer of fluid near a solid surface where the flow properties change rapidly, and it must be thin enough to fit meshing standards. Using structured meshes near walls causes the walls in the chamber to be typically flat and appropriate for the simulation of the viscous thin layer near the wall. The corner refinement method is used to improve solution accuracy in areas with sharp corners or edges. Cases with higher mesh density result in much finer velocity and pressure contours [13], using the mesh refinement technique to increase mesh density near the material surface.

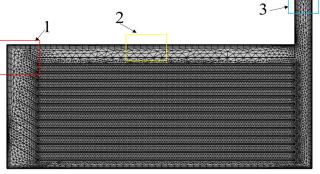
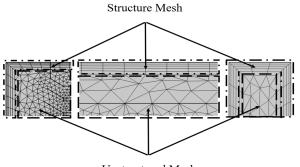


Fig. 2. Simulation mesh of chamber



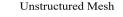
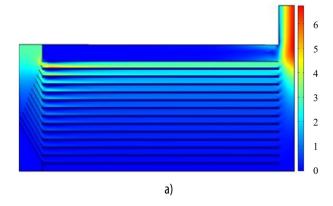


Fig. 3. Structured Mesh and Unstructured Mesh in the chamber

3. RESULT AND DISCUSSION



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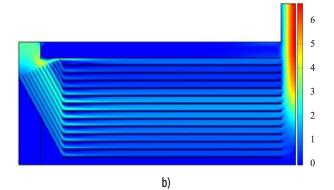


Fig. 4. a) d/i = 0; b) $d/i = \frac{1}{2}$

The chamber dryer is simulated in three cases with different ratios of air gap size (d) and inlet (i). The parameter d is changed, and i is constant.

∏ray d∕i	1	2	3	4	5	6	7
0	1.5109	1.0776	0.8224	0.6230	0.4899	0.3800	0.2982
1/2	0.3112	0.2444	0.2164	0.2507	0.4949	0.7091	0.7481
2/3	0.0184	0.0877	0.1574	0.2637	0.3321	0.4221	0.4353
Tray d/i	8	9	10	11	12	13	
0	0.2363	0.1871	0.1451	0.1038	0.0627	0.0310	
1/2	0.6523	0.5766	0.5086	0.4238	0.3718	0.3130	
2/3	0.4996	0.5252	0.5655	0.6368	0.6042	0.7729	

Table 1. Simulation results of AAVOMS (m/s)

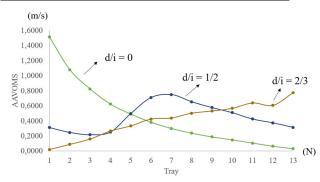


Fig. 5. AAVOMS on each tray in each d/i value

In case 1 (d/i = 0), tray 13 has minimum AAVOMS (0.0310m/s), and the first tray has maximum AAVOMS (1.5109m/s). When comparing case 2 (d/i = 1/2) to case 1, the minimum and maximum AAVOMS respectively change to tray 3 and tray 7; tray 1 has less air through the surface than in case 1 (lower AAVOMS). The final case (d/i = 2/3) is opposite to case 1: tray 1 has minimum AAVOMS (0.0184m/s), and tray 13 has maximum AAVOMS (0.7729m/s).

d/i	0	1/2	2/3
Nmax	1	7	13
Nmin	13	3	1
Diff.	12	-4	-12

Table 3. Criterion calculated for different d/i values

d/i Criterion	0	1/2	2/3
Va	0.4591	0.4478	0.4093
S _% (%)	96.80	40.76	55.34
Δ_{v}	3.2236	1.1873	1.8434

The criteria v_a decreases from 0.4591 at d/i = 0 to 0.4093 at d/i = 2/3. The v_a values at d/i = 0 and 1/2 are not significantly different, which means the amount of air through all material surfaces is approximately in these two cases.

The S_% value decreases from 96.80% to 40.76%, then increases to 55.34%. If d/i is more or less than 1/2, the relative variability of the AAVOMS set increases. Case 2 has the least relative variability of the AAVOMS set compared with other cases. The Δv value in this case significantly decreases, meaning the difference between the minimum and maximum values in the AAVOMS set decreases when d/i decreases. Δv is approximate in cases 2 and 3. It can be concluded that case 2 with d/i = 1/2 is the best among the others.

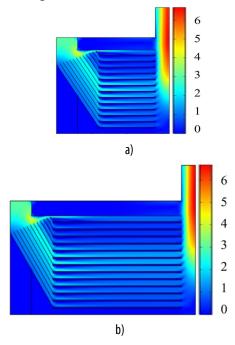


Fig. 6. Equipment length: a) 1500 mm; b) 2500 mm

The most appropriate d/i value (1/2) of all case studies above is used to improve the air uniformity of the equipment. Different equipment lengths (I): 1,500, 2,500, and 3,500 (mm) are simulated with the same boundary conditions as all cases above.

Table 4.	Simulation re	esults of av	verage v	elocity on	the material s	urface
(AAVOMS, m	/s)					

Tray I (mm)	1	2	3	4	5	6	7
1500	0.4984	0.3327	0.5463	0.7043	0.7167	0.6190	0.5260
2500	0.4777	0.5202	0.8024	0.8021	0.6733	0.5558	0.4561
3500	0.5362	0.7790	0.9144	0.7666	0.6144	0.4890	0.3964
Tray I (mm)	8	9	10	11	12	13	
1500	0.4441	0.3705	0.3126	0.2594	0.2109	0.1567	
2500	0.3775	0.3064	0.2543	0.2069	0.1596	0.1037	
3500	0.3183	0.2577	0.2059	0.1660	0.1196	0.0748	

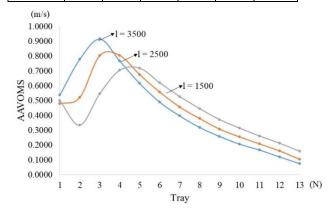


Fig. 7. AAVOMS on each tray in each case

 Table 5. Criterion calculated for different equipment length

l (mm) Criterion	1,500	2,500	3,500
Va	0.4383	0.4381	0.4337
S _% (%)	41.58	52.73	63.28
Δν	1.2777	1.5946	1.9357

Changing the equipment length changes the air distribution. The equipment height also affects the air distribution, but due to operational restrictions, it is limited. It is not necessary to consider the effect of the height of the equipment on the air distribution.

4. CONCLUSION

Despite installing, tuning, and finding out the best air blade angle value in the previous study which makes the

air distribution better, it can be improved more. In this study, the air gap size is tuned, and the most appropriate result is d/i = 1/2. It can be concluded that the bigger the air gap size, the better the air uniformity, as well as the better the final product quality (but if d/i exceeds $\frac{1}{2}$, the air distribution may be worse). After that, the air distribution is also evaluated by changing the trays and equipment length, and 1500mm is the best one.

In short, the whole study demonstrates the effect of the air blade angle, the air gap size (d) and the equipment length on the air uniformity in the chamber dryer. It also shows how to set the boundary conditions and mesh to obtain the best simulation results using COMSOL Multiphysics - a useful software for simulating. However, to approach the completely optimal design as well as apply it to the actual design, further research on 3D modeling is necessary.

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